

Hierarchically Porous Aminosilica Monolith as a CO₂ Adsorbent

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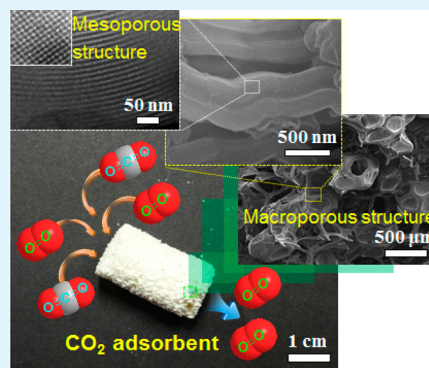
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ABSTRACT: A facile strategy is successfully developed for the centimeter-scale preparation of hierarchically porous aminosilica monolith as a CO₂ adsorbent just by simple processes of solvent-evaporation-induced coating, self-assembly, and concentration of tetraethyl orthosilicate sol on the surface of a polymer foam template without any adhesive composite material or hydrothermal treatment. (3-Aminopropyl) trimethoxysilane is immobilized on the surface of silica monolith via a gas-phase procedure. The silica frameworks of the monolith mimic those of the polymer foam template at the macroscale, and the frameworks are composed of the SBA-15 structure at the nanoscale. The hierarchically porous structure demonstrates improved properties over the single-mode porous component, with the macroporous framework ensuring mechanical stability and good mass transport properties, while the smaller pores provide the functionality for CO₂ adsorption.

KEYWORDS: hierarchical structures, aminosilica, porous materials, pressure drop, CO₂ capture



1. INTRODUCTION

The CO₂ emissions associated with human activities are mainly due to the burning of fossil fuels and various chemical processes.¹ Currently, over 85% of the global energy demand is being supported by the burning of fossil fuels.² As the CO₂ levels in the atmosphere continue to increase, considerable concern has been raised regarding the impact of CO₂ emissions on the environment and its contribution to global climate change.³ CO₂ capture is the most practical method to reduce CO₂ emission in the atmosphere.⁴ In CO₂ capture processes, adsorption on solid media is considered as one of the most efficient methods owing to the regeneration with low energy.⁵ In solid adsorbents, amines-modified porous materials have been found to be a viable option for effective CO₂ adsorbent owing to no corrosion of equipment, the adsorption/desorption process at atmospheric pressure, the low energy consumption for the adsorbent regeneration, the high adsorption capacity, and no loss of the adsorbent.^{6–10}

Various types of amines-immobilized high surface area silica materials have been widely used for CO₂ capture.¹¹ However, despite the dramatic advantages of mesoporous materials, preparation of materials with simultaneous control of morphology and pore structure in different length scales still remains a challenging task.¹² Preparation of a hierarchically porous silica monolith (HPSM) has attracted much attention to make up for the weakness of the mesoporous silica materials as support materials.^{13–18} In the HPSM structure, mesopores can provide adsorption sites for the CO₂ capture, whereas the existence of macropores can offer a highway for CO₂ accessing

the sites with small pressure drops.¹⁹ Therefore, fabrication of the HPSM has been the central core of researcher's interest. However, reported processes for fabrication of the HPSM demanded additional adhesive composite materials,²⁰ complicate process such as fabrication of highly ordered colloidal crystal template,²¹ or a pressurizing process in an autoclave (hydrothermal treatment).²² In these processes, complete removal of the template materials and additional adhesive composite materials is very important after the calcination process because the residual carbonaceous composites can cover the surface of HPSM and disrupt the immobilization of functional groups on the silica surface. In this study, HPSM has been fabricated simply just by processes of solvent-evaporation-induced coating, self-assembly, and concentration of tetraethyl orthosilicate (TEOS) sol on the surface of a polyurethane (PU) foam template without any adhesive composite material or complicate process. We were also able to freely manufacture the HPSM with the desired PU-template form.

As a functional group for CO₂ capture, (3-aminopropyl) trimethoxysilane (APTMS) was immobilized on the surface of HPSM (HPSM–NH₂) via a gas-phase procedure to increase the uniform surface density of amino groups on the silica surface.²³ HPSM–NH₂ showed higher CO₂ adsorption capacity than APTMS-immobilized SBA-15 at both room temperature (~25 °C) and high temperature (100 °C) because

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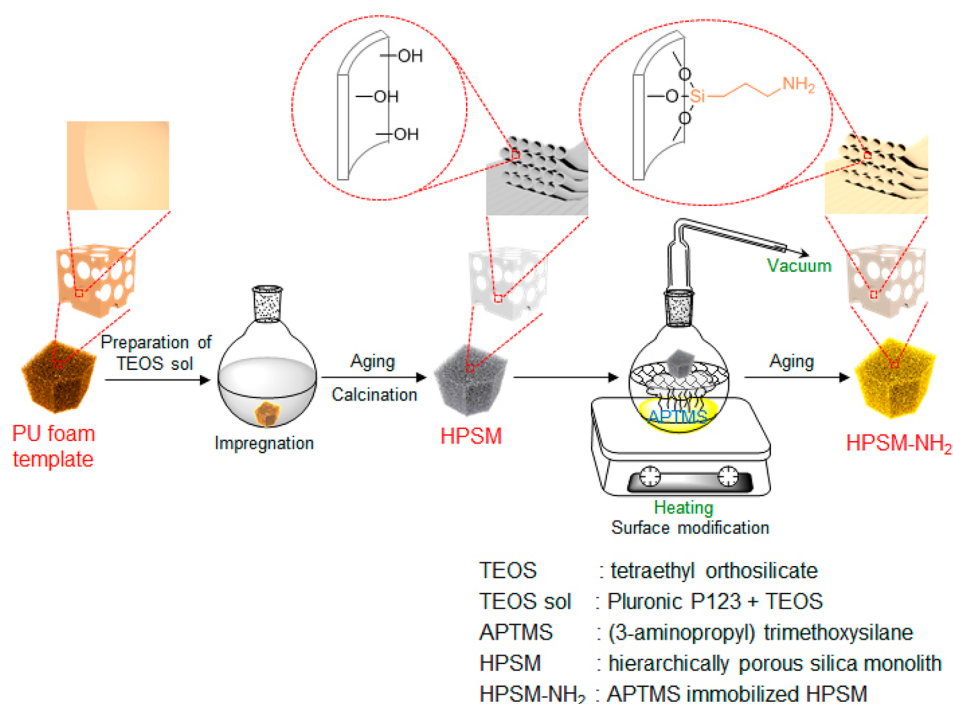


Figure 1. Schematic illustration of the preparation of the hierarchically porous aminosilica monolith (HPSM-NH₂).

the macropore in HPSM-NH₂ allows higher mass transport of CO₂ in the structure than the mesopore does. The pressure drop of the HPSM-NH₂ packed column was also approximately 36 times lower than that of the APTMS-immobilized SBA-15 packed column. In addition, molecular structure and composition information from the uppermost layers of the surface of HPSM-NH₂ were obtained by time-of-flight secondary ion mass spectrometry (ToF-SIMS).

In this study, we focused our efforts on development of the simple fabrication of a hierarchically porous aminosilica monolith to improve the CO₂ adsorption capacity, to make the CO₂ adsorbent for the desired shape and size, and to reduce the pressure drop in the CO₂ adsorption process.

2. EXPERIMENTAL SECTION

2.1. Reagents and Chemicals. All reagents and solvents were of AR grade and used without further purification unless otherwise noted. Polyurethane (PU) foam was purchased from LG sponge (Korea). Pluronic P123 triblock copolymer (EO₂₉-PO₇₀-EO₂₀), tetraethylorthosilicate (TEOS), and (3-aminopropyl) trimethoxysilane (APTMS) were bought from Aldrich. The 2 N HCl solution was purchased from Fluka. Deionized water (DI water) was obtained using a Milli-Q water system (18.2 MΩ·cm).

2.2. Preparation of Hierarchically Porous Silica Monolith (HPSM). HPSM was prepared from the prehydrolyzed TEOS, Pluronic P123, and a PU foam template. A 4.0 g amount of Pluronic P123 was dissolved in 30 g of DI water and 120 g of 2 N HCl solution, and the solution was well stirred for 5 h at 60 °C. Then, 8.5 g of TEOS was added slowly with stirring, and the resulting mixture was then kept at 24 h at 60 °C. Afterward, the clear supernatant liquid of the mixture solution was removed to concentrate the TEOS solution. The obtained solution was coated onto the PU foam template (1.5 × 1.5 × 1.5 cm³). The air bubbles inside the PU foam template were removed by frequently squeezing the PU foam template during infusion of the concentrated sol solution. The infused PU foam template was kept in an 80 °C oven for 48 h followed by calcination with a nitrogen purge at 550 °C for 5 h to remove the Pluronic P123 and the PU template completely, and the hierarchically porous silica monolith was obtained. The silica monolith was named as HPSM.

2.3. Synthesis of Amino-Functionalized HPSM (HPSM-NH₂).

APTMS was deposited onto HPSM using a gas-phase technique. Prior to deposition, the HPSM was pretreated at 150 °C in order to remove physisorbed water molecules from the silica surface. The pressure in the APTMS (5 mL) contained reactor was 10–50 mbar while vaporizing the APTMS. The APTMS in the reactor was vaporized at 120 °C for 24 h. The reaction temperature and reaction time were high enough to avoid condensation of the APTMS molecules onto the pore walls. For removal of unreacted reactants, the reaction was followed by a nitrogen purge at the reaction temperature. In addition, amino-functionalized HPSM was dried using a freeze drier (5 mTorr) for 1 week. The amino-functionalized silica monolith was named as HPSM-NH₂.

2.4. Characterization. High-resolution X-ray diffraction (XRD) patterns were obtained using a Rigaku D/max-2500 V/PC diffractometer with a high-power Cu Kα source (40 kV and 150 mA). Field emission gun scanning electron microscopy (FEG-SEM) measurements were taken on a FEI Inspect F50 at 15 kV. An elemental analyzer (EA 1108, FISON Instruments) was used to measure the nitrogen amount of HPSM-NH₂. Transmission electron microscopy (TEM) images were obtained with a Philips CM-30 operating at 200 kV. Nitrogen adsorption/desorption isotherms were measured with an ASAP2420 sorption analyzer (Micromeritics). Prior to determination of the adsorption isotherm, the sample was evacuated at 1.333 Pa and 423.15 K for 2 h to remove all physisorbed species from the surface of the adsorbent. The Brunauer–Emmett–Teller (BET) method was used to determine the surface area. Pore size distributions were calculated by the Barrett–Joyner–Halenda (BJH) method. To analyze the surface of HPSM-NH₂, negative time-of-flight secondary ion mass spectrometry (ToF-SIMS) was carried out in the mass range of 0.5–400 *m/z* using an ION-TOF TOF-SIMS 5 system. Mass spectra were obtained using a Bi₃⁺ liquid metal ion source (1 pA pulsed ion current) from an area of 100 μm × 100 μm. The mass resolution measured on the Si[±] signal of a silicon wafer was *m/Δm* = 4000 in the negative mode. Fourier transform infrared (FT-IR) spectroscopy (Frontier, PerkinElmer) was used to confirm the synthesis of HPSM-NH₂. Samples were blended with KBr and then pressed into disks for analysis.

2.5. Carbon Dioxide Adsorption. CO₂ adsorption/desorption measurements for HPSM-NH₂ were performed using a thermogravi-

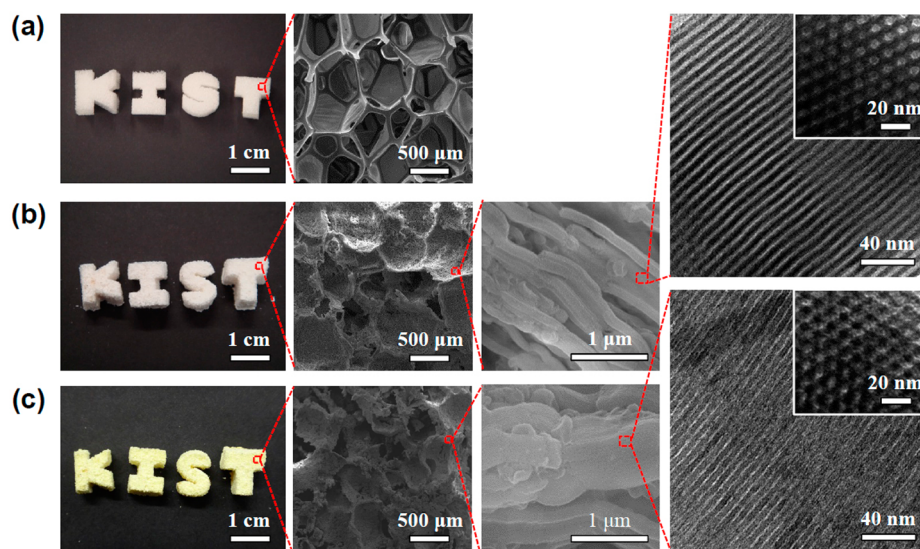


Figure 2. Representative photograph, FEG-SEM, and TEM images of the hierarchically porous structures from low magnification to high magnification. (a) PU foam template, (b) hierarchically porous silica monolith (HPSM), and (c) APTMS-immobilized HPSM (HPSM-NH₂).

metric analyzer (TGA). A sample weight of ca. 10 mg was loaded into an alumina sample pan in a TG unit (SCINCO thermal gravimeter S-1000) and tested for CO₂ adsorption/desorption performances. Initial activation of the samples was carried out at 110 °C for 3 h in a nitrogen atmosphere. An adsorption run was then conducted using dehumidified CO₂ gas (99.9%, Shinyang Oxygen Industry Co., Korea) at 28, 50, 75, and 100 °C under atmospheric pressure, and the desorption pressure was performed at 110 °C for 3 h. Both CO₂ and N₂ were passed through an automatic valve, assisted with a timer for continuous adsorption and desorption profile. The silica gel blue (Daejung Chemicals Co., Korea) packed columns were used to remove the moisture in CO₂ and N₂ gases.

2.6. Pressure Drop Measurement. In pressure drop experiments, 0.45 g of HPSM-NH₂ was packed into the adsorption column (i.d. 7.6 mm × length 80 mm). A 0.45 g amount of SBA-15-NH₂ was used for comparison (i.d. 7.6 mm × length 60 mm). The pressure drop between the inlet and the outlet of the column was measured under various velocities of dehumidified CO₂ gas (0–0.15 m/s) at a room temperature.

3. RESULTS AND DISCUSSION

3.1. Synthesis of HPSM-NH₂. Formation of amino-functionalized HPSM (HPSM-NH₂) was fabricated using the process of solvent-evaporation-induced self-assembly. The process is mainly composed of five steps: preparation and concentration of TEOS sol, impregnation of polyurethane (PU) template, aging and calcination, surface modification, and aging (Figure 1). In the first step, Pluronic P123 triblock copolymer (EO₂₉-PO₇₀-EO₂₀) forms a cylindrical micelle structure, and TEOS adsorbs onto the cylindrical micelle structure (CMS). In the second step, TEOS/CMS composite adsorbs onto the surface of the PU foam template. In the third step, solvent evaporation (induced coating and self-assembly) occurs and hierarchically porous silica monolith (HPSM) forms after calcination. In the fourth step, aminosilane (APTMS) is deposited onto HPSM through a gas-phase technique. After deposition of aminosilane on the surface of HPSM, individual aminosilane can incorporate with the surface of HPSM via (i) covalent bonding with attached aminosilanes on HPSM, (ii) direct covalent bonding with HPSM, (iii) multilayer formation with neighboring aminosilanes by vertical and horizontal polymerization, (iv) intermolecularly hydrogen bonding with

amine group or HPSM surface silanol group, and (v) noncovalent bonding such as ionic or electrostatic attraction. For regeneration of the CO₂ adsorbent, the structure of v should be avoided because the structure is too weak to endure the regeneration process.^{24–27} This causes loss of CO₂ adsorption capacity of the adsorbent during the CO₂ adsorption–desorption cycling process. Therefore, deposition was followed by a nitrogen purge at the deposition temperature and freeze drying under vacuum for removal of unreacted aminosilanes. In the final step, the deposited aminosilane binds to the surface of HPSM tightly and forms a covalent bond.

The significant advantage of our hierarchically porous silica monolith (HPSM) is that the monolith can be made in almost any shape. It depends only on the shape of the template. In this study, a PU foam was used as the template. The first initials of the research institute (KIST, Korea Institute of Science and Technology) was fabricated in three dimensions with the PU foam as shown in Figure 2a. The range of the pore size in the PU foam template is 300–800 μm. After the processes of solvent-evaporation-induced self-assembly of the TEOS sol solution, aging, and calcination, the walls of the giant pores (300–800 μm) had an open periodic mesoporous structure which was confirmed by transmission electron microscopy (TEM) images (Figure 2b). Highly ordered parallel lines were able to be observed in the TEM image, relating to a hexagonal arrangement of mesopores (side view). In the inset images, the uniform hexagonal mesostructure could be seen from the perpendicular view to the pore channel axis. An intricate, well-ordered meso–macroporous solid, in which all pore scales are interconnected, was produced via solvent-evaporation-induced self-assembly of the TEOS sol solution, aging, and calcination. Even after deposition of the aminosilane (APTMS) onto the surface of the HPSM, all meso–macropores were well interconnected as shown in Figure 2c.

The N₂ adsorption/desorption isotherms of HPSM and HPSM-NH₂ are presented in Figure 3a. All samples showed a typical type IV N₂ adsorption isotherm with pronounced capillary condensations reflecting internal mesopores and interparticle voids between the primary particles.²⁸ However, each sample showed different hysteresis. The HPSM displayed a type of IV isotherm with H1 hysteresis and a sharp increase in

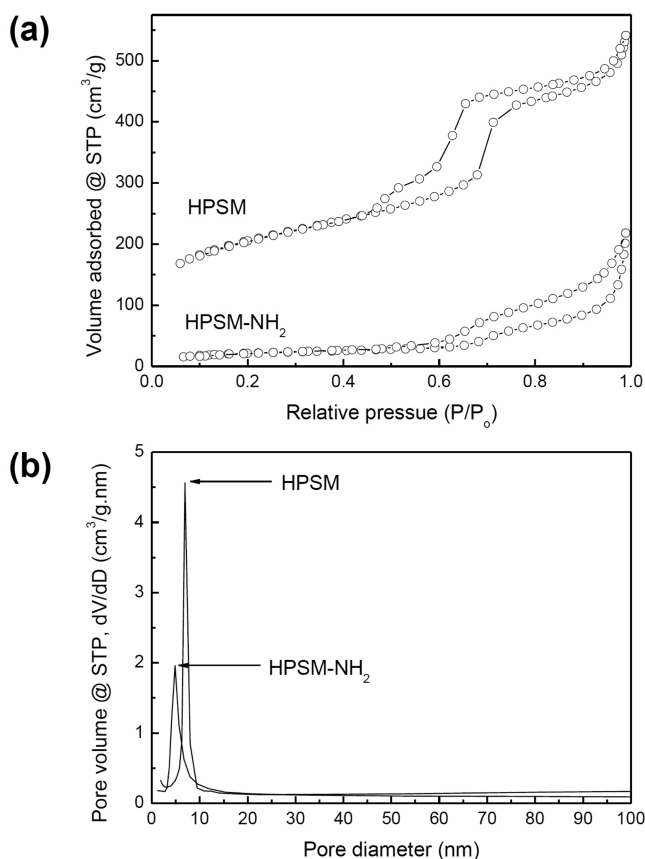


Figure 3. Textural characterization of hierarchically porous silica monoliths. (a) N_2 adsorption/desorption isotherms, and (b) pore size distributions of HPSM and HPSM-NH₂.

volume adsorbed at $P/P_0 \approx 0.68$, characteristic of highly ordered mesoporous materials. However, capillary condensation of N_2 occurred over a slightly wider P/P_0 range in APTES-functionalized HPSM (HPSM-NH₂) than in HPSM because of heterogeneous mesopores in HPSM-NH₂. After surface functionalization of HPSM, the surface of the mesopores in HPSM became heterogeneous while the surface of mesopores in unmodified HPSM was homogeneous. The HPSM pore diameter distribution showed a narrow pore size distribution as shown in Figure 3b. However, HPSM-NH₂ showed slightly broader and lower intensity than HPSM in the pore size distribution curves. The textural properties of the samples are summarized in Table 1. HPSM presented a high value of specific surface area (726.40 m²/g) and 8.38 nm pore diameter. HPSM-NH₂ showed lower values of textural properties (specific surface area 312.15 m²/g, pore diameter: 5.26 nm) than HPSM.

Structural characterization by X-ray diffraction (XRD) reveals that the frameworks of HPSM are composed of the ordered

Table 1. Textural Properties of APTMS Immobilized HPSM and SBA-15

materials	specific surface area (BET) [m ² /g]	pore diameter (BJH) [nm]
HPSM	726	8.38
HPSM-NH ₂	312	5.26
SBA-15	873	5.29
SBA-15-NH ₂	288	3.09

mesoporous arrangement of the typical SBA-15 structure (Figure 4). The XRD pattern at low angle corresponding to

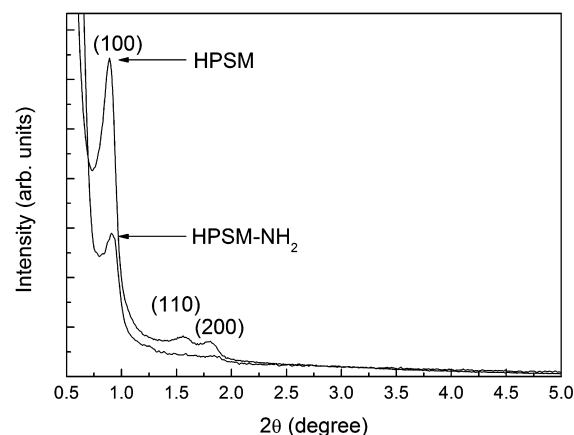


Figure 4. XRD patterns of HPSM and HPSM-NH₂.

the HPSM shows a typical profile of a 2D-hexagonal structure with $P6mm$ plane group of SBA-15. The XRD pattern of HPSM displays a very intense peak (100) and two additional high-order peaks (110, 200). This XRD pattern reveals that the wall of HPSM consists of the hexagonal structure of SBA-15.²⁹ The hexagonal structure was clearly shown in the TEM image of HPSM (see Figure 2b). It should be noted that the decrease in (100) intensity for HPSM-NH₂ provides evidence of APTMS grafting occurring mainly inside the mesopore channels, since attachment of APTMS to the surface of the mesopore channels reduces the XRD intensity of the amorphous silica wall.

Incorporation of the aminosilane in the silica frameworks can be qualitatively confirmed by the FT-IR spectra shown in Figure 5. To remove adsorbed gas and water molecules, HPSM

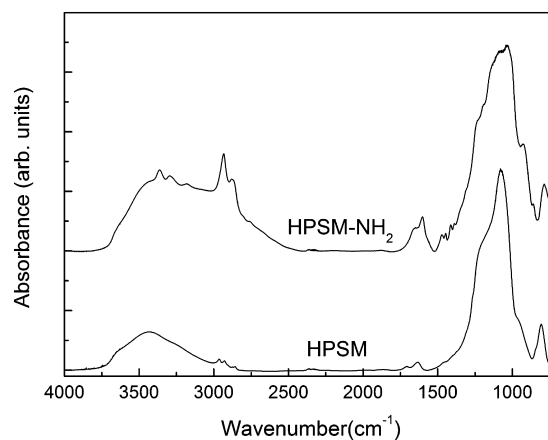


Figure 5. FT-IR spectra of HPSM and HPSM-NH₂.

and HPSM-NH₂ were dried at 110 °C under vacuum for 3 days and quickly analyzed with a FT-IR spectrometer. After modification of HPSM with APTMS (HPSM-NH₂), the new peaks appeared at 3358, 3297, 2935, 2882, and 1603 cm⁻¹ for NH₂ asymmetric stretching, NH₂ symmetric stretching, CH₂ asymmetric stretching, CH₂ symmetric stretching, and NH₂ deformation, respectively. The newly appearing peaks demonstrate that APTMS was successfully immobilized on the surface of HPSM.

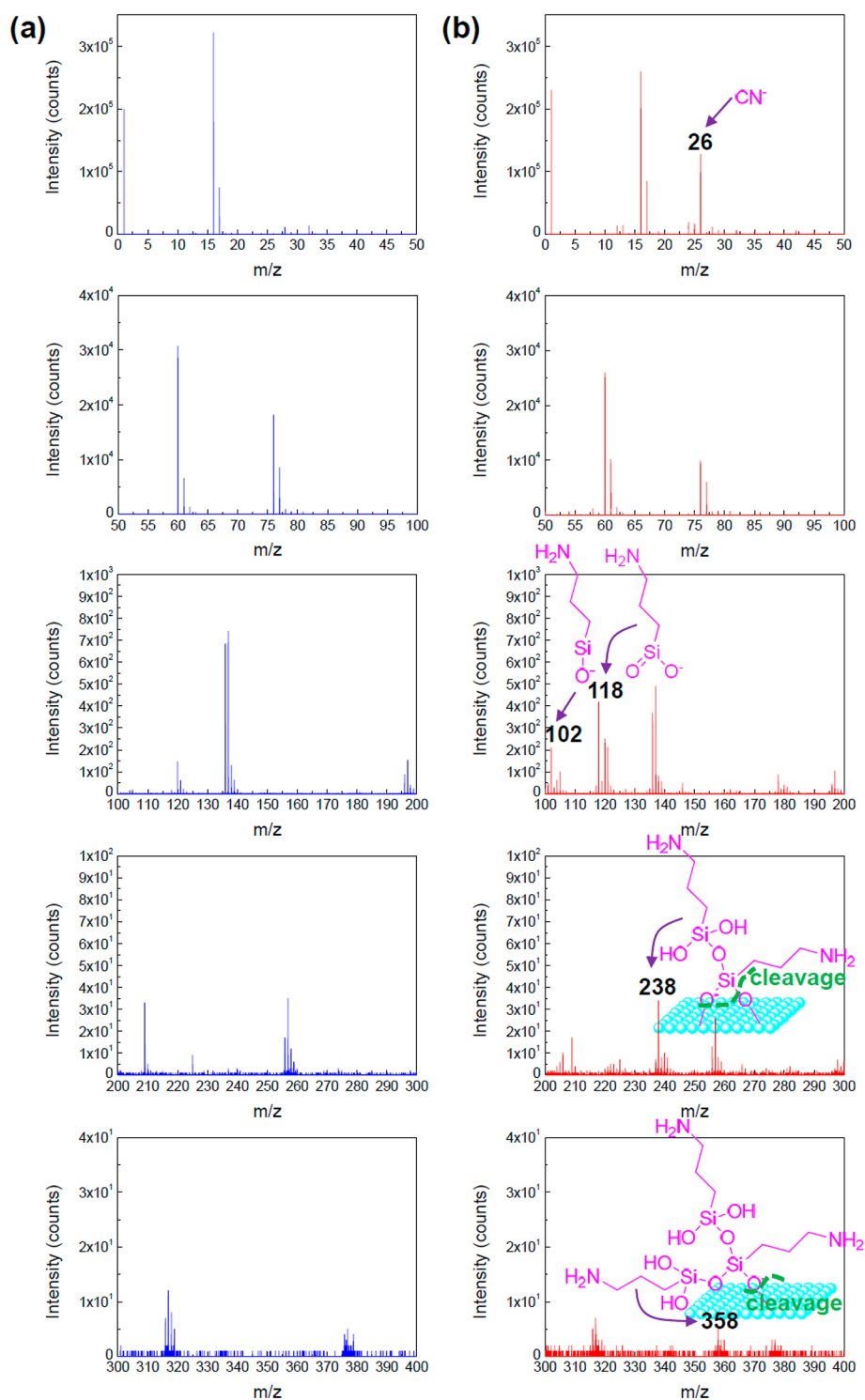


Figure 6. Negative ToF-SIMS spectra of (a) HPSM and (b) HPSM-NH₂.

3.2. Surface Characterization of HPSM-NH₂ with ToF-SIMS. After immobilization of APTMS on HPSM, the pore diameter of mesopores in HPSM decreased from ca. 8.38 to ca. 5.26 nm (see Table 1). Therefore, the increased wall thickness of the mesopores is ca. 1.56 nm. If APTMS is immobilized on the surface of the HPSM as a monolayer state, maximum increased thickness of HPSM-NH₂ is approximately 0.9 nm theoretically due to the ca. 0.9 nm of the APTMS molecular length.³⁰ This result indicates that APTMS multilayers were incorporated onto the surface of HPSM. ToF-SIMS technique

provides molecular structure and composition information from the uppermost layers of surfaces. Negative-ion ToF-SIMS spectra of HPSM and HPSM-NH₂ are shown in Figure 6. After immobilization of APTMS on the surface of HPSM (Figure 6b), the major peaks at m/z 26, 102, and 118 amu correspond to CN⁻, C₃H₈ONSi⁻, and C₃H₈O₂NSi⁻, respectively. These fragments are the APTMS fingerprints, since they are present in the spectrum due to fragmentation of the APTMS molecule. Interestingly, the specific peaks appearing at 238 and 358 amu correspond to the fragments of the

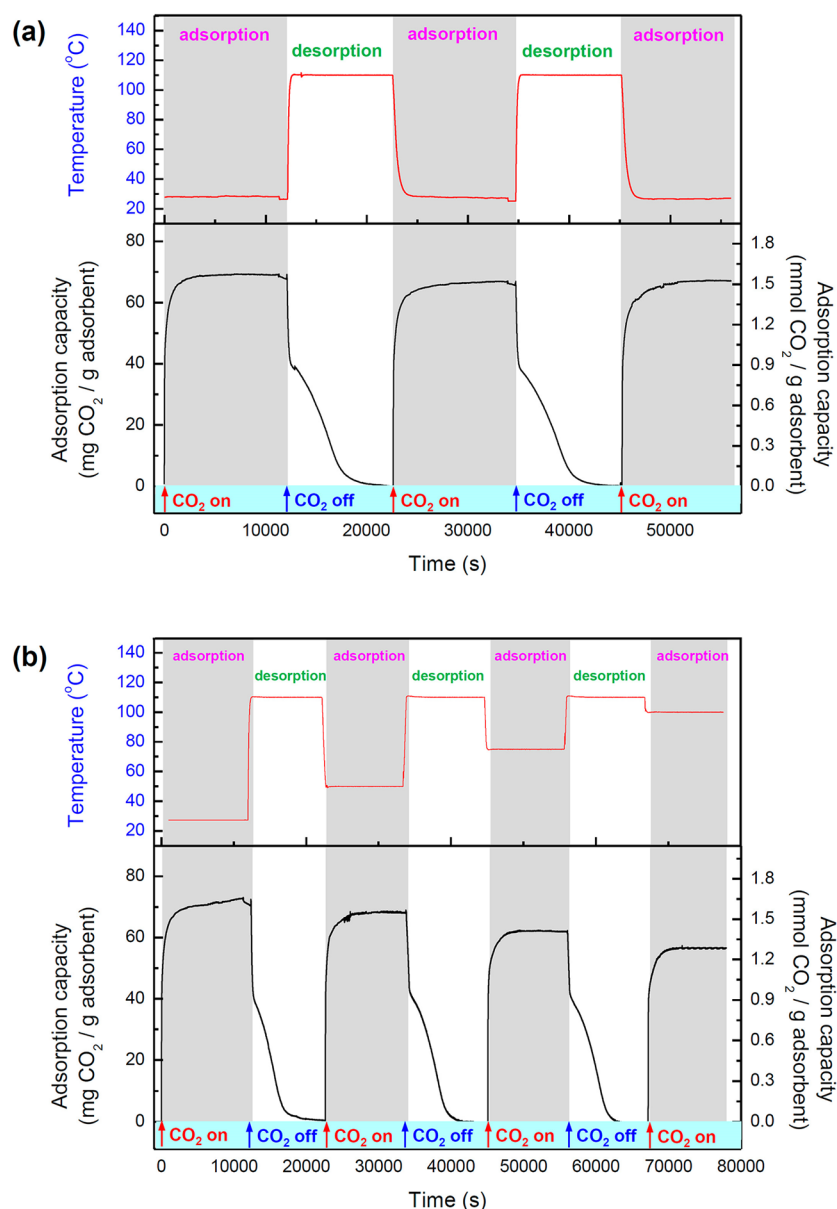


Figure 7. CO₂ adsorption/desorption cycles on HPSM–NH₂ (a) at isothermal adsorption temperature and (b) at different adsorption temperatures (28, 50, 75, and 100 °C).

polyaminosilanes. These peaks indicate that the APTMS multilayer formation owing to horizontal and vertical polymerization formed during immobilization of APTMS on the surface of HPSM.

3.3. CO₂ Adsorption/Desorption on Modified HPSM.

To evaluate the CO₂ adsorption capacity on HPSM–NH₂, the repeated CO₂ adsorption/desorption performances were conducted. The adsorption performance was carried out at 28 °C at atmospheric pressure with pure CO₂ gas, and the desorption performance was conducted at 110 °C at atmospheric pressure with N₂ gas. In this adsorption/desorption performance, the maximum CO₂ adsorption value (1.51 mmol/g) was stable during the cycle process owing to complete removal of CO₂ from HPSM–NH₂ in the desorption process (Figure 7a). The percentage loss of adsorption capacity of HPSM–NH₂ was less than 1% for 3 cycles. Sayari et al. reported the high loss of adsorption capacity was observed in the case of CO₂ adsorption–desorption cycling experiment

under dry conditions, while the loss was very low under humid conditions.^{10,31} Although we did only 3 cycles for the adsorption–desorption cycling experiment, the loss was very low under dry conditions. HPSM–NH₂ did not exhibit high adsorption capacity; however, it showed good stability of the regeneration under dry conditions.

To compare the value of the maximum CO₂ adsorption capacity of HPSM–NH₂ with other CO₂ adsorbent, APTMS-immobilized SBA-15 (SBA-15–NH₂) was prepared according to our previous report.³² Textural properties (specific surface area and pore diameter) of the synthesized SBA-15 and SBA-15–NH₂ are summarized in Table 1. Surface properties of HPSM–NH₂ and SBA-15–NH₂ as a CO₂ adsorbent are listed in Table 2. The number of APTMS molecules in HPSM–NH₂ was calculated using the loaded amount of nitrogen (3.78 mmol/g) and the BET specific surface area of HPSM and SBA-15 for HPSM–NH₂ and SBA-15–NH₂ respectively, and the values for HPSM–NH₂ and SBA-15–NH₂ were 3.13 and 2.31

Table 2. Comparison of APTMS Immobilized HPSM and SBA-15

materials	N amount in adsorbent [mmol/g]	no. of molecules (APTMS) per area [# /nm ²]	adsorption capacity of CO ₂ [mmol/g]	adsorbed CO ₂ per N [mmol/mmol]
HPSM-NH ₂	3.78	3.13	1.51	0.39
SBA-15-NH ₂	3.43	2.31	0.95	0.27

/nm² respectively. Primary amine can incorporate with CO₂ to make carbamate via the zwitterionic intermediate formation. Caplow reported carbamate formation through the zwitterionic intermediate, and other research groups developed it.³³ The mechanism was later summarized well by Choi et al. that the lone pair on the amine attacks the carbon of CO₂ to produce the zwitterion, and then free base deprotonates the zwitterion to form the carbamate.⁵ Thus, the maximum amine efficiency of an amine adsorbent is 0.5 mol of CO₂ per mol of N under dry conditions. In addition to amine groups for the CO₂ capture agent, a hydroxyl group on the silica surface can influence CO₂ adsorption.^{34–38} Amine efficiency, defined here as the number of CO₂ captured per mass unit divided by the moles of N per mass unit, gives a reflection of the adsorbent's efficiency in perspective with its potential. Here, the CO₂ adsorption performance was conducted at dry conditions, and the amine efficiency of HPSM-NH₂ was 0.39 mmol/mmol. In theory, CO₂ incorporates with two primary amines at dry conditions.³⁹ However, the obtained amine efficiency of the HPSM-NH₂ indicated a lower value than 0.5 of the theoretical one. The geographical and steric effects can cause isolation of some amines, which can serve the role of CO₂ capturing. Therefore, the adsorption capacity value from the CO₂ adsorption experiment is lower than the theoretical one. However, the value of HPSM-NH₂ is higher than that of SBA-15-NH₂ owing to the hierarchically porous structure of HPSM-NH₂. The macropore allows higher mass transport of CO₂ in the structure than the mesopore does.

Figure 7b shows the CO₂ adsorption/desorption cycles of HPSM-NH₂ at different adsorption temperatures. It can be observed that the CO₂ adsorption capacity of HPSM-NH₂ at 100 °C (1.28 mmol/g) is lower than that at 28 °C (1.51 mmol/

g). Adsorption of CO₂ on the porous adsorbent consists of two steps: (i) CO₂ adsorption on the surface of adsorbent and (ii) CO₂ diffusion from the surface into the pores of the adsorbent. Thermodynamic and dynamic factors are the main parameters influencing the adsorption capacity.⁴⁰ However, these factors are mutually vying. Increasing the temperature has both positive and negative influences on the CO₂ adsorption capacity, that is, to enhance the diffusion of CO₂ favoring adsorption but to enhance decomposition of ammonium carbonate disfavoring adsorption. Although the increase of the adsorption temperature is not favorable to enhancement of the CO₂ adsorption capacity of HPSM-NH₂, its CO₂ adsorption capacity is less influenced by the temperature than that of previously reported SBA-15-NH₂ due to hierarchical pores in its structure for good CO₂ diffusion.³² Therefore, this result leads to the conclusion that CO₂ diffusion is not the dominant parameter reducing CO₂ adsorption on HPSM-NH₂ in comparison to the thermodynamic factor.

3.4. Pressure Drop. Pressure drop is one of the significant parameters in industrial processes. Macropores in hierarchically porous structures would provide easier access to the active sites and reduce the pressure drop over the materials.^{41–45} Figure 8 shows the pressure drop across packed beds of HPSM-NH₂ and SBA-15-NH₂ at various superficial velocities. The pressure drop per unit length was calculated by dividing the experimental results over the length of the corresponding bed. It can be anticipated that components possessing hierarchical porosity demonstrate to possess improved properties over single-mode porous components, with the macroporous framework ensuring mechanical stability and good mass transport properties (such as a higher rate of external transfer of mass and lower pressure drop), while the smaller pores provide the functionality for CO₂ adsorption. This was confirmed by the low pressure drop recorded per unit length of bed of HPSM-NH₂, which was approximately 36 times lower than the pressure drop per unit length of bed of SBA-15-NH₂.

4. CONCLUSIONS

In summary, we demonstrated the facile fabrication of hierarchically porous aminosilica monolith (HPSM-NH₂) as a CO₂ adsorbent using the PU foam template, tetraethyl orthosilicate (TEOS), triblock copolymer (Pluronic P123), and

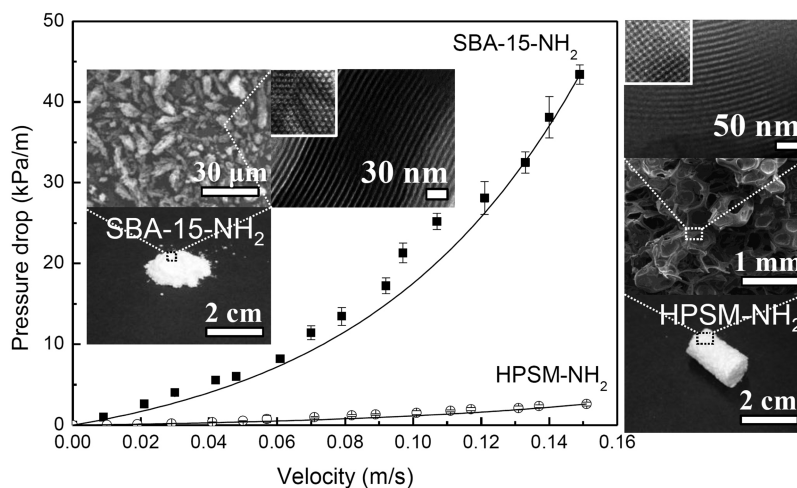


Figure 8. Pressure drop along adsorption columns packed with SBA-15-NH₂ and HPSM-NH₂ (insets; photograph, FEG-SEM, and TEM images of used SBA-15-NH₂ and HPSM-NH₂ for the CO₂ adsorption column). Data are presented as mean \pm standard deviation, $n = 5$.

(3-aminopropyl) trimethoxysilane (APTMS). Hierarchically porous silica monolith (HPSM) was fabricated simply just by solvent-evaporation-induced coating, self-assembly, and concentration of TEOS sol on the surface of the polyurethane (PU) template without any adhesive composite material or pressurizing process. We were able to freely manufacture the hierarchically porous aminosilica monolith with the desired PU-template shape. APTMS was immobilized on the surface of HPSM (HPSM-NH₂) via a gas-phase procedure to increase the surface density of amino groups on the silica. It was confirmed by TEM and XRD analysis that the walls of macropores in HPSM, the silica frameworks, are composed of SBA-15. ToF-SIMS results indicated that the multilayers owing to APTMS polymerization occurred during immobilization of APTMS on the surface of HPSM (HPSM-NH₂), although monolayers also formed on the surface. These multilayers can influence the CO₂ adsorption capacity of HPSM-NH₂. The prepared HPSM-NH₂ showed not only slightly higher CO₂ capture amount but also slightly higher efficiency for CO₂ capture than SBA-15-NH₂. The synthesized HPSM-NH₂ depends on the adsorption temperature that the CO₂ adsorption capacity of HPSM-NH₂ was high at the low adsorption temperature. The purpose behind the design of the hierarchically porous structure is to improve the flow resistance and pressure drop. It is noteworthy that the pressure drop of HPSM-NH₂ was approximately 36 times lower than that of SBA-15-NH₂.

The prepared HPSM can be a promising support for immobilization of functional groups for specific purposes. We believe that our HPSM-NH₂ can be applied to various applications such as CO₂ capture, sequestration of heavy metal ions, radionuclides capture, etc.

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Notes

The authors declare no competing financial interest.

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